

Chapter 5

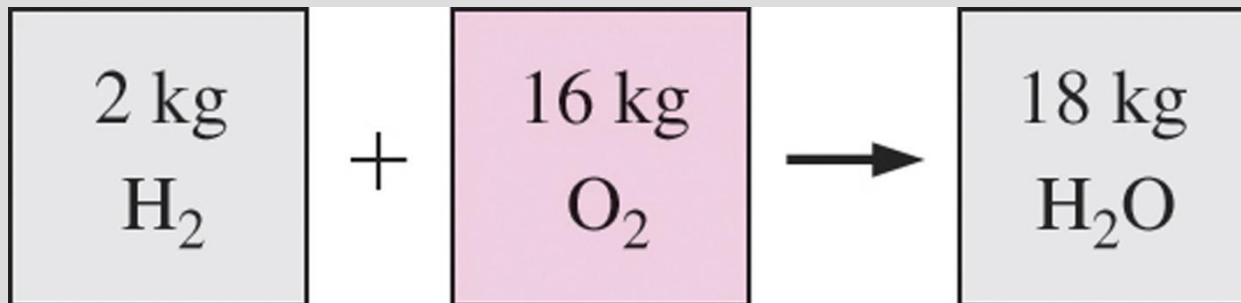
MASS AND ENERGY ANALYSIS OF CONTROL VOLUMES

CONSERVATION OF MASS

Conservation of mass: Mass, like energy, is a conserved property, and it cannot be created or destroyed during a process.

Closed systems: The mass of the system remain constant during a process.

Control volumes: Mass can cross the boundaries, and so we must keep track of the amount of mass entering and leaving the control volume.



Mass is conserved even during chemical reactions.

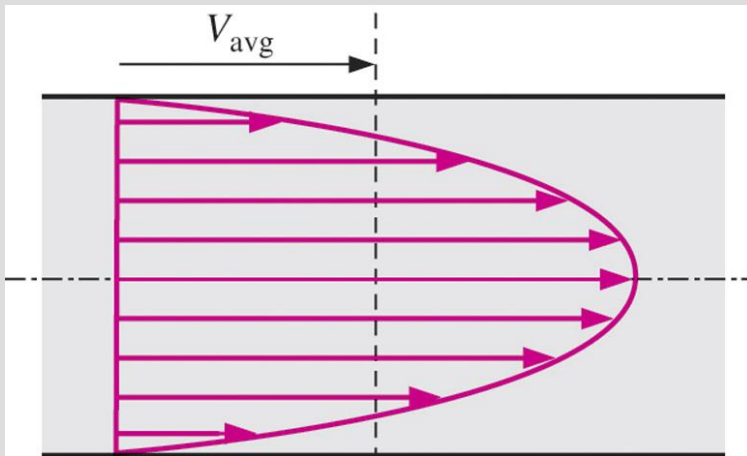
Mass and Volume Flow Rates

$$\delta \dot{m} = \rho V_n dA_c$$

$$\dot{m} = \int_{A_c} \delta \dot{m} = \int_{A_c} \rho V_n dA_c$$

$$\dot{m} = \rho V_{\text{avg}} A_c \quad (\text{kg/s})$$

$$\dot{m} = \rho \dot{V} = \frac{\dot{V}}{v} \quad \text{Mass flow rate}$$



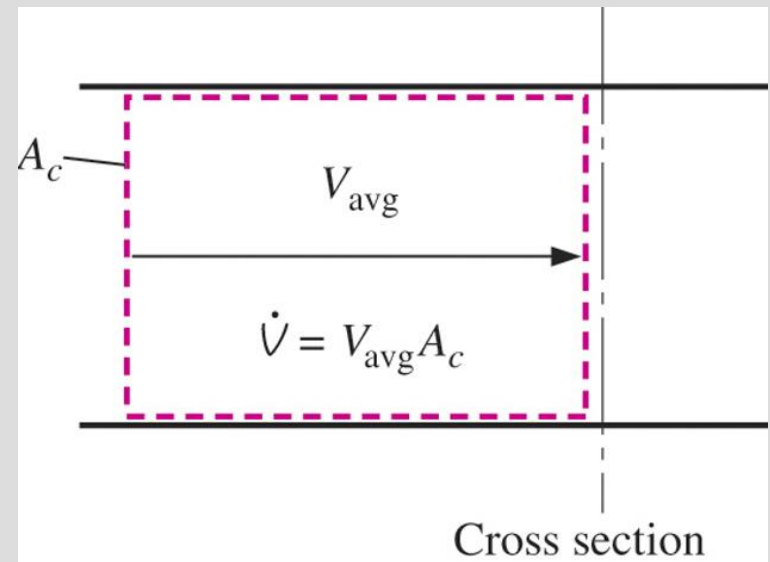
The average velocity V_{avg} is defined as the average speed through a cross section.

$$V_{\text{avg}} = \frac{1}{A_c} \int_{A_c} V_n dA_c$$

Definition of average velocity

Volume flow rate

$$\dot{V} = \int_{A_c} V_n dA_c = V_{\text{avg}} A_c = V A_c \quad (\text{m}^3/\text{s})$$



The volume flow rate is the volume of fluid flowing through a cross section per unit time.

Conservation of Mass Principle

The conservation of mass principle for a control volume: The net mass transfer to or from a control volume during a time interval Δt is equal to the net change (increase or decrease) in the total mass within the control volume during Δt .

$$\left(\begin{array}{c} \text{Total mass entering} \\ \text{the CV during } \Delta t \end{array} \right) - \left(\begin{array}{c} \text{Total mass leaving} \\ \text{the CV during } \Delta t \end{array} \right) = \left(\begin{array}{c} \text{Net change in mass} \\ \text{within the CV during } \Delta t \end{array} \right)$$



$$m_{in} - m_{out} = \Delta m_{CV} \quad (\text{kg})$$

$$\sum m_{in} - \sum m_{out} = \Delta m_{CV}$$

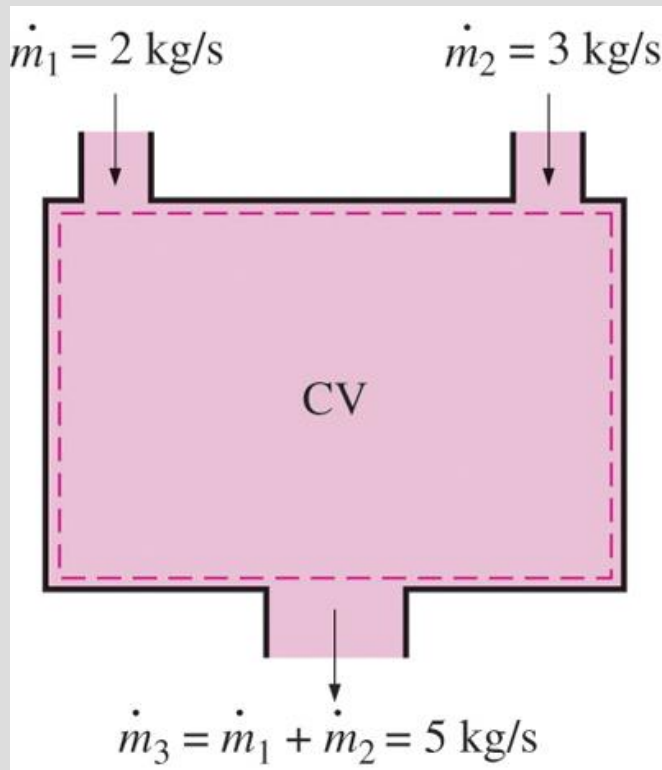
$$\dot{m}_{in} - \dot{m}_{out} = dm_{CV}/dt \quad (\text{kg/s})$$

$$\sum \dot{m}_{in} - \sum \dot{m}_{out} = dm_{CV}/dt$$

Mass Balance for Steady-Flow Processes

During a steady-flow process, the total amount of mass contained within a control volume does not change with time ($m_{CV} = \text{constant}$).

Then the conservation of mass principle requires that **the total amount of mass entering a control volume equals the total amount of mass leaving it.**



For steady-flow processes, we are interested in the amount of mass flowing per unit time, that is, *the mass flow rate*.

$$\sum_{\text{in}} \dot{m} = \sum_{\text{out}} \dot{m} \quad (\text{kg/s}) \quad \text{Multiple inlets and exits}$$

$$\dot{m}_1 = \dot{m}_2 \rightarrow \rho_1 V_1 A_1 = \rho_2 V_2 A_2 \quad \text{Single stream}$$

Many engineering devices such as nozzles, diffusers, turbines, compressors, and pumps involve a single stream (only one inlet and one outlet).

Conservation of mass principle for a two-inlet–one-outlet steady-flow system.

Special Case: Incompressible Flow

- **Incompressible Flow.** A flow in which the specific volume (and density) remain constant.
- The conservation of mass relations can be simplified even further when the fluid is incompressible, which is usually the case for liquids.

$$\sum_{\text{in}} \dot{V} = \sum_{\text{out}} \dot{V} \quad (\text{m}^3/\text{s})$$

Steady,
incompressible

$$\dot{V}_1 = \dot{V}_2 \rightarrow V_1 A_1 = V_2 A_2$$

Steady,
incompressible
flow (single stream)

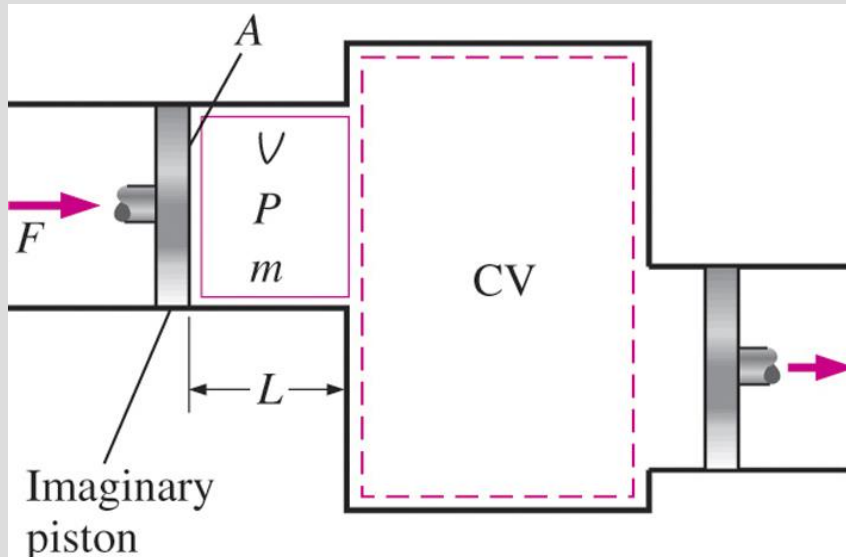
FLOW WORK AND THE ENERGY OF A FLOWING FLUID

Flow work, or flow energy: The work (or energy) required to push the mass into or out of the control volume. This work is necessary for maintaining a continuous flow through a control volume.

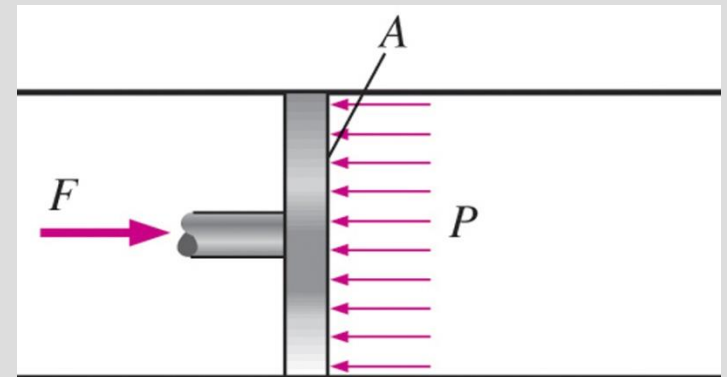
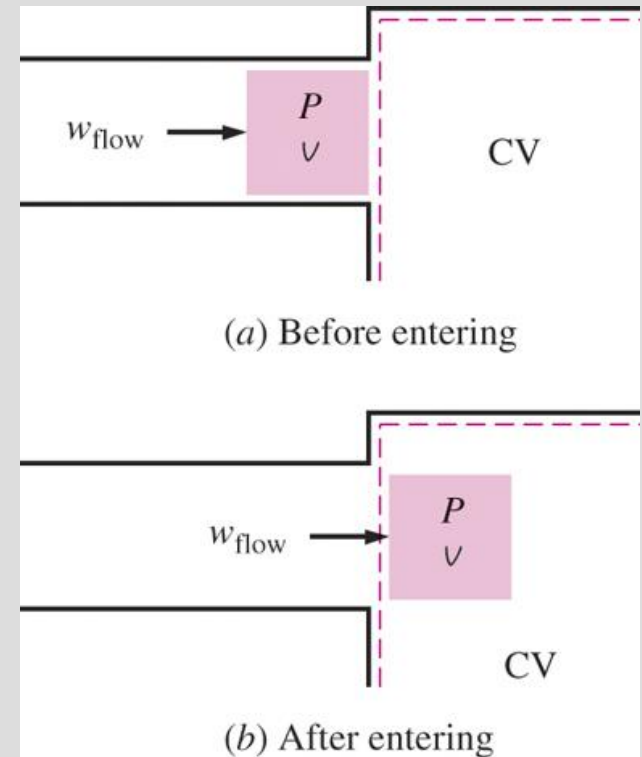
$$F = PA$$

$$W_{\text{flow}} = FL = PAL = PV \quad (\text{kJ})$$

$$w_{\text{flow}} = Pv \quad (\text{kJ/kg})$$



Schematic for flow work.



In the absence of acceleration, the force applied on a fluid by a piston is equal to the force applied on the piston by the fluid.

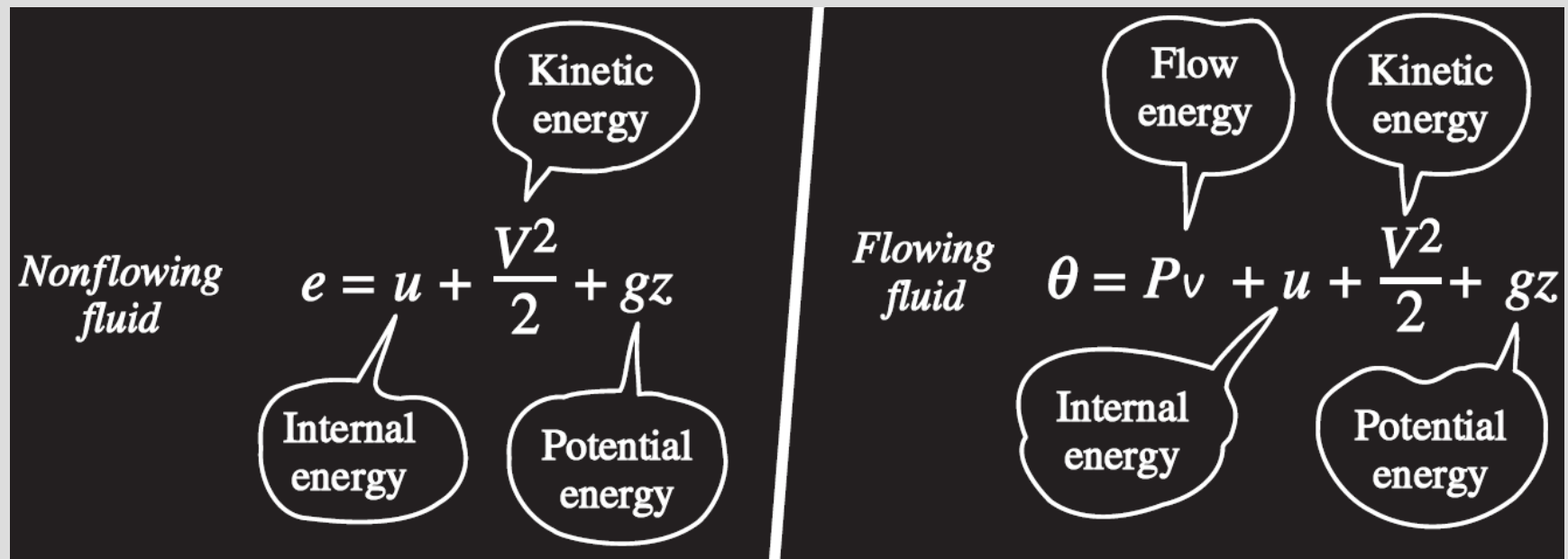
Total Energy of a Flowing Fluid

$$e = u + \text{ke} + \text{pe} = u + \frac{V^2}{2} + gz \quad (\text{kJ/kg})$$

$$\theta = P_v + e = P_v + (u + \text{ke} + \text{pe}) \quad h = u + P_v$$

$$\theta = h + \text{ke} + \text{pe} = h + \frac{V^2}{2} + gz \quad (\text{kJ/kg})$$

The flow energy is automatically taken care of by enthalpy. In fact, this is the main reason for defining the property enthalpy.

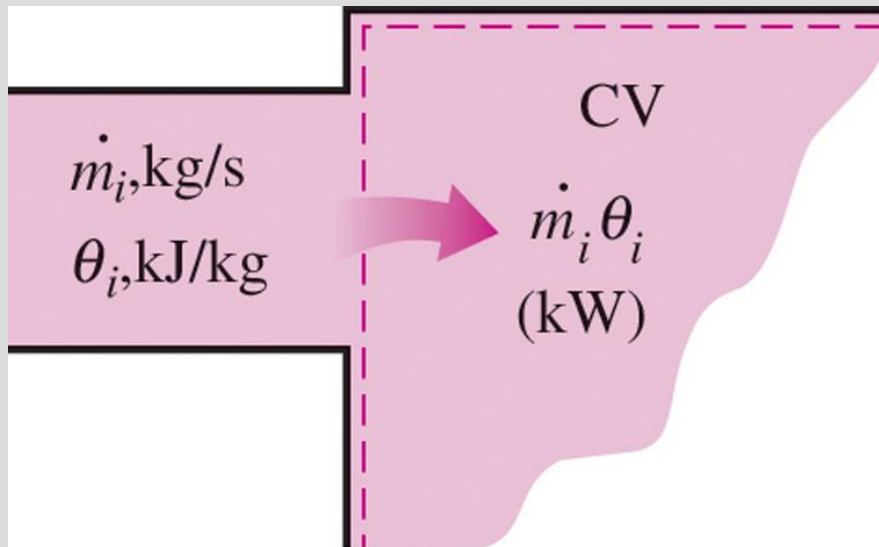


The total energy consists of three parts for a nonflowing fluid and four parts for a flowing fluid.

Energy Transport by Mass

Amount of energy transport: $E_{\text{mass}} = m\theta = m\left(h + \frac{V^2}{2} + gz\right)$ (kJ)

Rate of energy transport: $\dot{E}_{\text{mass}} = \dot{m}\theta = \dot{m}\left(h + \frac{V^2}{2} + gz\right)$ (kW)



When the kinetic and potential energies of a fluid stream are negligible

$$E_{\text{mass}} = mh$$

$$\dot{E}_{\text{mass}} = \dot{m}h$$

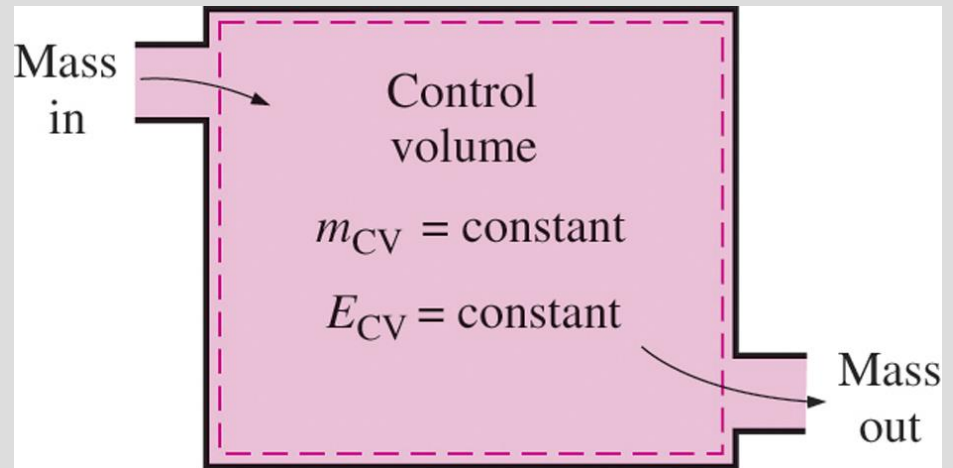
The product $\dot{m}_i \theta_i$ is the energy transported into control volume by mass per unit time.

ENERGY ANALYSIS OF STEADY-FLOW SYSTEMS

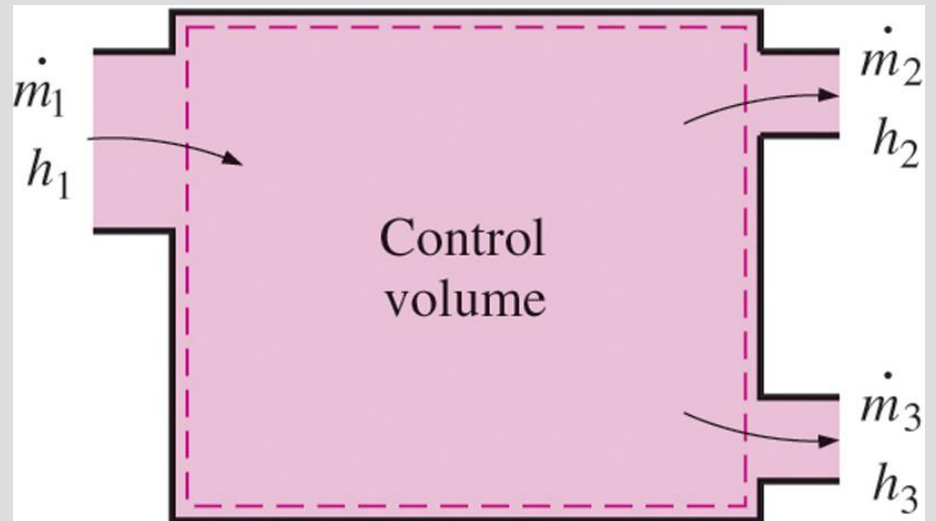


Many engineering systems such as power plants operate under steady conditions.

Under steady-flow conditions, the fluid properties at an inlet or exit remain constant (do not change with time).



Under steady-flow conditions, the mass and energy contents of a control volume remain constant.



Mass and Energy balances for a steady-flow process

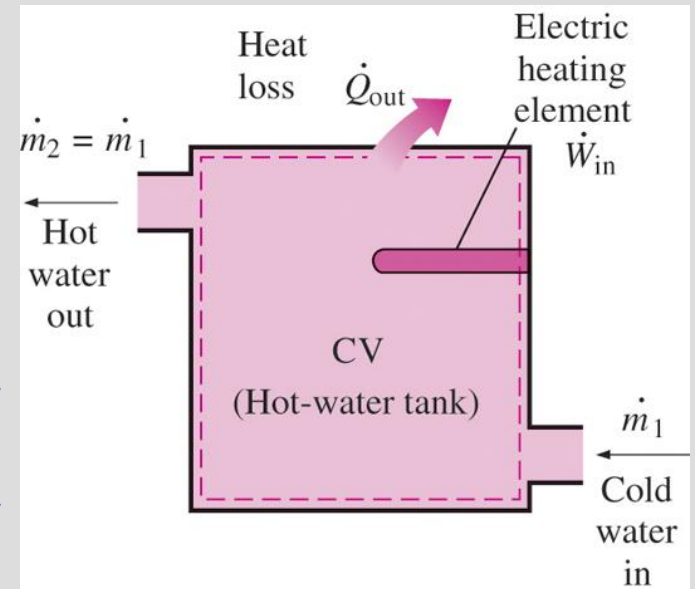
$$\sum_{\text{in}} \dot{m} = \sum_{\text{out}} \dot{m} \quad (\text{kg/s})$$

$$\dot{m}_1 = \dot{m}_2$$

$$\rho_1 V_1 A_1 = \rho_2 V_2 A_2$$

Mass
balance

A water
heater in
steady
operation.



Energy
balance

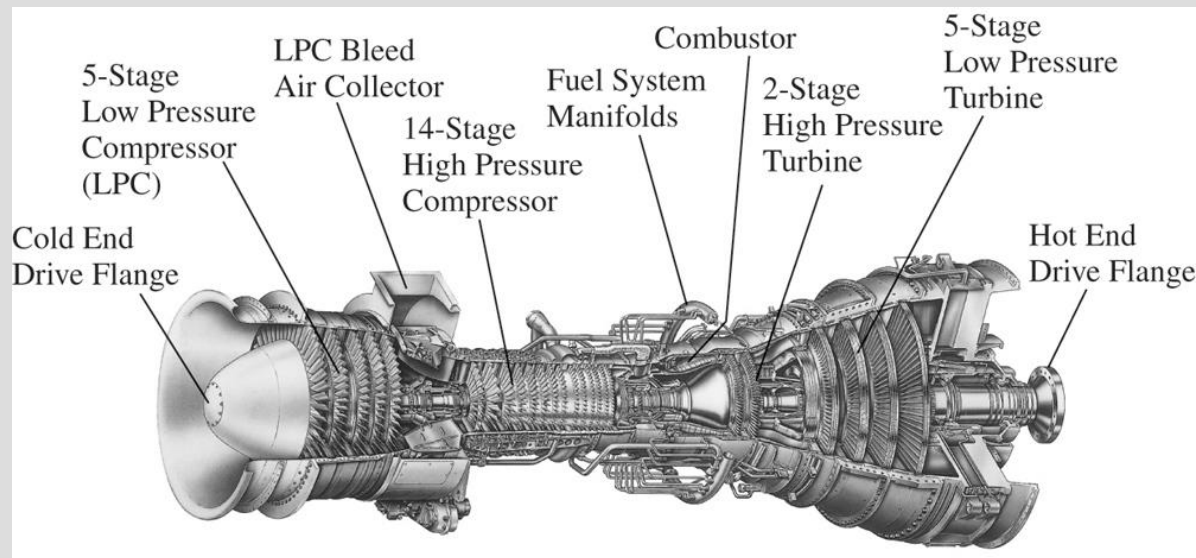
$$\underbrace{\dot{E}_{\text{in}} - \dot{E}_{\text{out}}}_{\text{Rate of net energy transfer by heat, work, and mass}} = \underbrace{\frac{dE_{\text{system}}}{dt}}_{\text{Rate of change in internal, kinetic, potential, etc., energies}} \xrightarrow{0 \text{ (steady)}} 0$$

$$\underbrace{\dot{E}_{\text{in}}}_{\text{Rate of net energy transfer in by heat, work, and mass}} = \underbrace{\dot{E}_{\text{out}}}_{\text{Rate of net energy transfer out by heat, work, and mass}} \quad (\text{kW})$$

$$\dot{Q}_{\text{in}} + \dot{W}_{\text{in}} + \underbrace{\sum_{\text{in}} \dot{m} \left(h + \frac{V^2}{2} + gz \right)}_{\text{for each inlet}} = \dot{Q}_{\text{out}} + \dot{W}_{\text{out}} + \underbrace{\sum_{\text{out}} \dot{m} \left(h + \frac{V^2}{2} + gz \right)}_{\text{for each exit}}$$

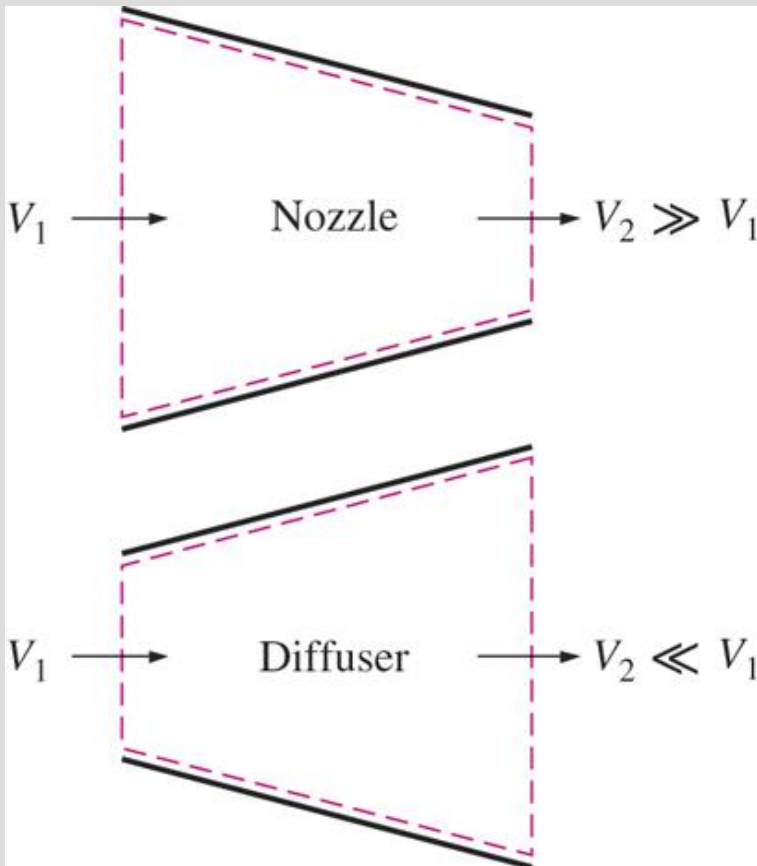
SOME STEADY-FLOW ENGINEERING DEVICES

Many engineering devices operate essentially under the same conditions for long periods of time. The components of a steam power plant (turbines, compressors, heat exchangers, and pumps), for example, operate nonstop for months before the system is shut down for maintenance. Therefore, these devices can be conveniently analyzed as steady-flow devices.



A modern land-based gas turbine used for electric power production. This is a General Electric LM5000 turbine. It has a length of 6.2 m, it weighs 12.5 tons, and produces 55.2 MW at 3600 rpm with steam injection.

Nozzles and Diffusers



Nozzles and diffusers are shaped so that they cause large changes in fluid velocities and thus kinetic energies.

Nozzles and diffusers are commonly utilized in jet engines, rockets, spacecraft, and even garden hoses.

A **nozzle** is a device that *increases the velocity of a fluid* at the expense of pressure.

A **diffuser** is a device that *increases the pressure of a fluid* by slowing it down.

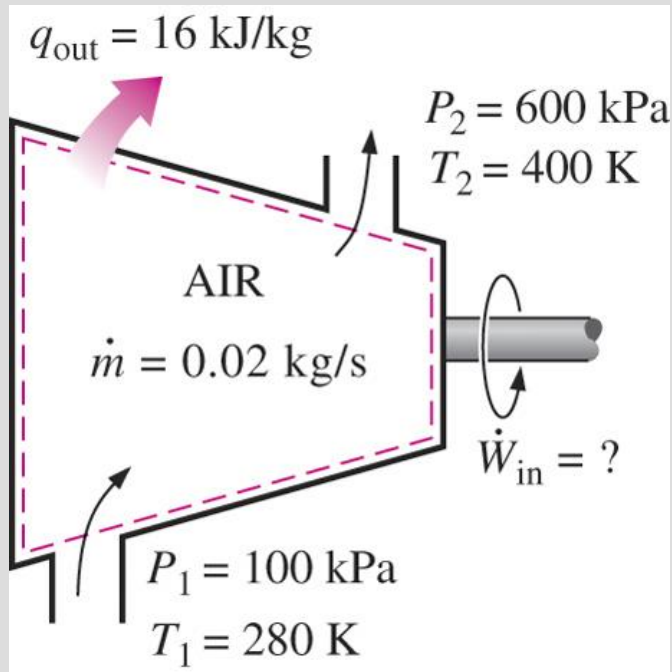
The cross-sectional area of a nozzle decreases in the flow direction for subsonic flows and increases for supersonic flows. The reverse is true for diffusers.

Energy
balance for
a nozzle or
diffuser:

$$\dot{E}_{\text{in}} = \dot{E}_{\text{out}}$$
$$\dot{m} \left(h_1 + \frac{V_1^2}{2} \right) = \dot{m} \left(h_2 + \frac{V_2^2}{2} \right)$$

(since $\dot{Q} \cong 0$, $\dot{W} = 0$, and $\Delta p_e \cong 0$)

Turbines and Compressors



Energy balance for the compressor in this figure:

$$\dot{E}_{\text{in}} = \dot{E}_{\text{out}}$$
$$\dot{W}_{\text{in}} + \dot{m}h_1 = \dot{Q}_{\text{out}} + \dot{m}h_2$$

(since $\Delta \text{ke} = \Delta \text{pe} \cong 0$)

Turbine drives the electric generator in steam, gas, or hydroelectric power plants.

As the fluid passes through the turbine, work is done against the blades, which are attached to the shaft. As a result, the shaft rotates, and the turbine produces work.

Compressors, as well as **pumps** and **fans**, are devices used to increase the pressure of a fluid. Work is supplied to these devices from an external source through a rotating shaft.

A **fan** increases the pressure of a gas slightly and is mainly used to mobilize a gas.

A **compressor** is capable of compressing the gas to very high pressures.

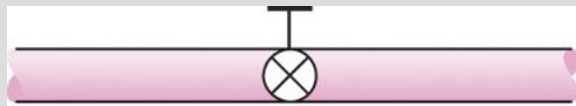
Pumps work very much like compressors except that they handle liquids instead of gases.

Throttling valves

Throttling valves are *any kind of flow-restricting* devices that cause a significant pressure drop in the fluid.

What is the difference between a turbine and a throttling valve?

The pressure drop in the fluid is often accompanied by a *large drop in temperature*, and for that reason throttling devices are commonly used in refrigeration and air-conditioning applications.



(a) An adjustable valve



(b) A porous plug



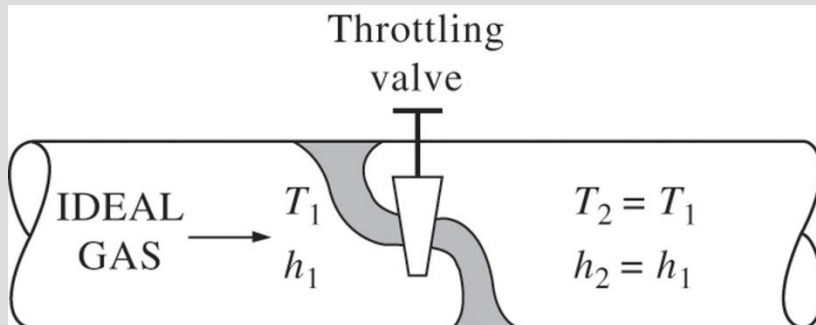
(c) A capillary tube

Energy
balance

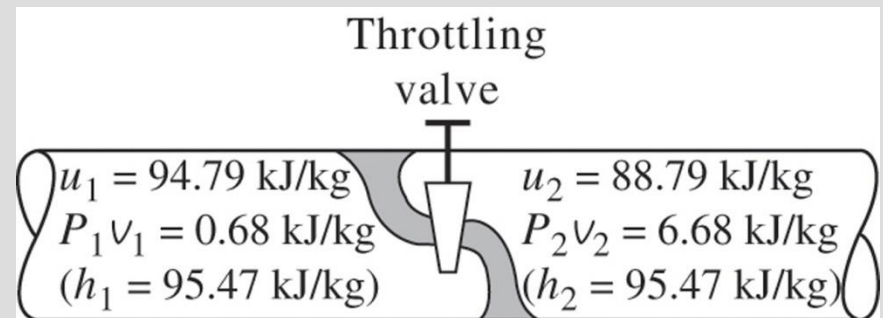
$$h_2 \cong h_1$$

$$u_1 + P_1 v_1 = u_2 + P_2 v_2$$

Internal energy + Flow energy = Constant



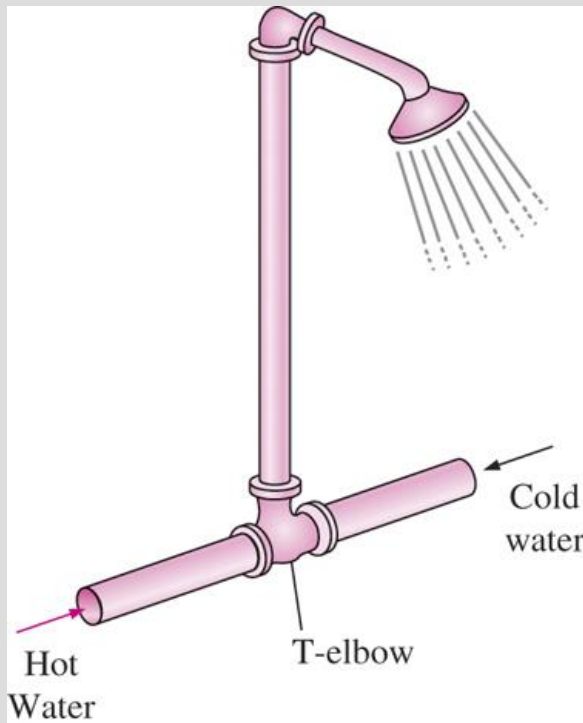
The temperature of an ideal gas does not change during a throttling ($h = \text{constant}$) process since $h = h(T)$.



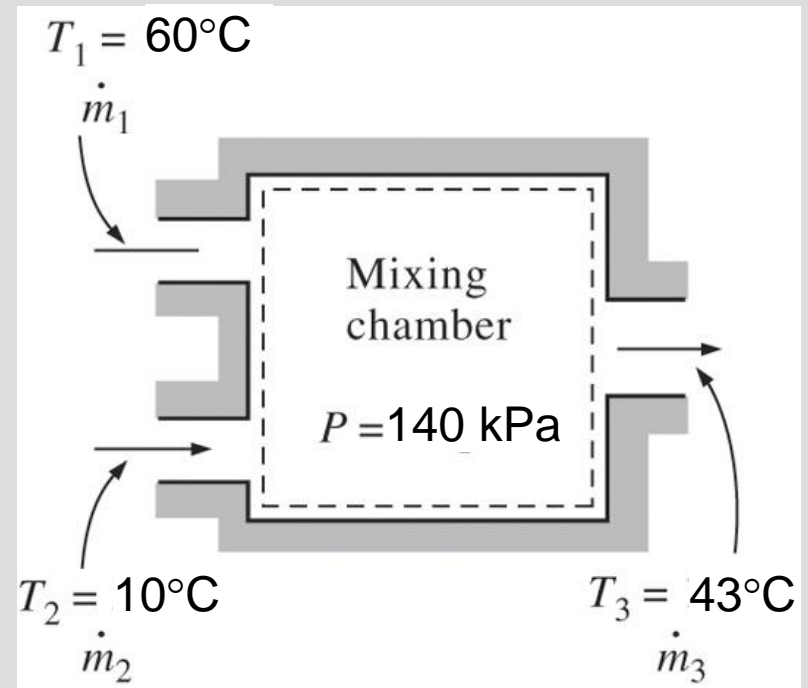
During a throttling process, the enthalpy of a fluid remains constant. But internal and flow energies may be converted to each other.

Mixing chambers

In engineering applications, the section where the mixing process takes place is commonly referred to as a **mixing chamber**.



The T-elbow of an ordinary shower serves as the mixing chamber for the hot- and the cold-water streams.



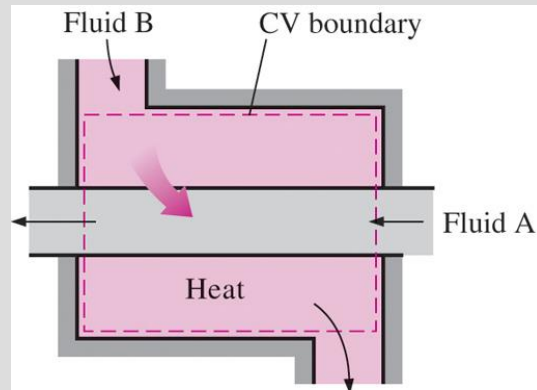
Energy balance for the adiabatic mixing chamber in the figure is:

$$\dot{E}_{\text{in}} = \dot{E}_{\text{out}}$$
$$\dot{m}_1 h_1 + \dot{m}_2 h_2 = \dot{m}_3 h_3$$

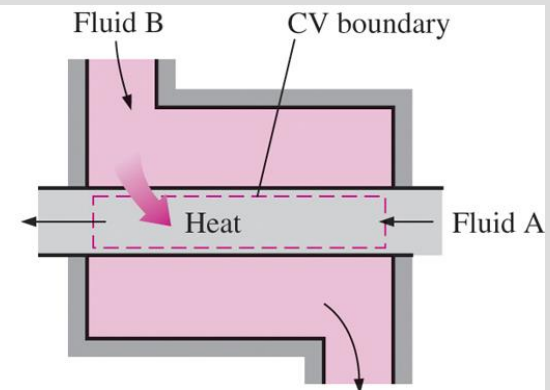
(since $\dot{Q} \cong 0$, $\dot{W} = 0$, $ke \cong pe \cong 0$)

Heat exchangers

Heat exchangers are devices where two moving fluid streams exchange heat without mixing. Heat exchangers are widely used in various industries, and they come in various designs.

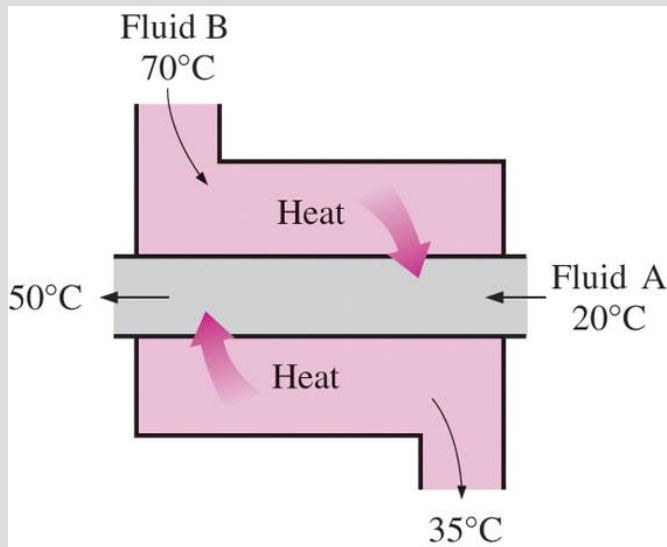


(a) System: Entire heat exchanger ($Q_{CV} = 0$)



(b) System: Fluid A ($Q_{CV} \neq 0$)

The heat transfer associated with a heat exchanger may be zero or nonzero depending on how the control volume is selected.



A heat exchanger can be as simple as two concentric pipes.

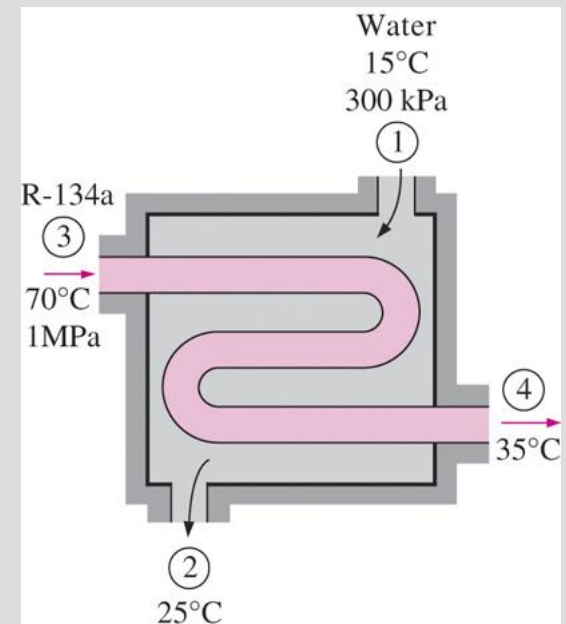
Mass and energy balances for the adiabatic heat exchanger in the figure is:

$$\dot{m}_1 = \dot{m}_2 = \dot{m}_w$$

$$\dot{m}_3 = \dot{m}_4 = \dot{m}_R$$

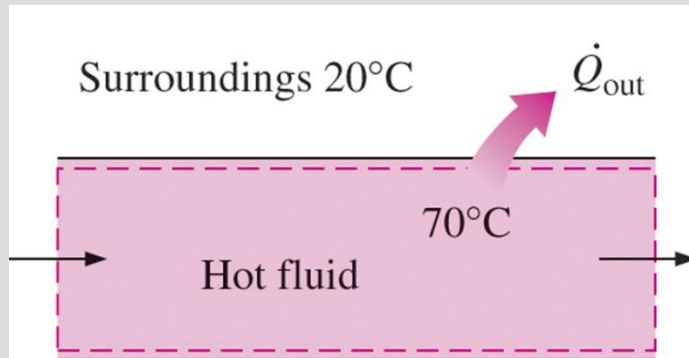
$$\dot{E}_{in} = \dot{E}_{out}$$

$$\dot{m}_1 h_1 + \dot{m}_3 h_3 = \dot{m}_2 h_2 + \dot{m}_4 h_4$$



Pipe and duct flow

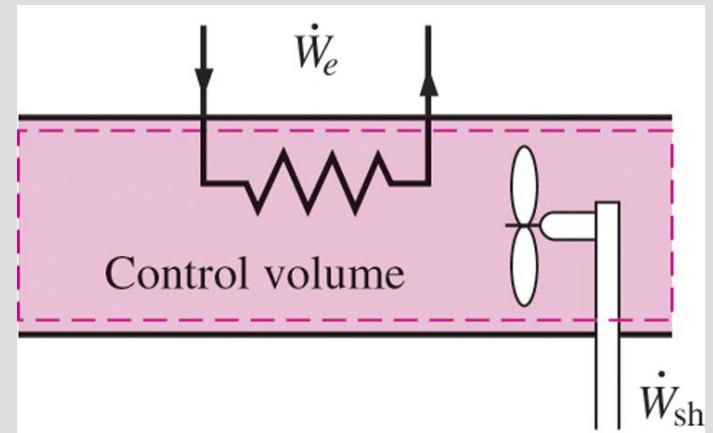
The transport of liquids or gases in pipes and ducts is of great importance in many engineering applications. Flow through a pipe or a duct usually satisfies the steady-flow conditions.



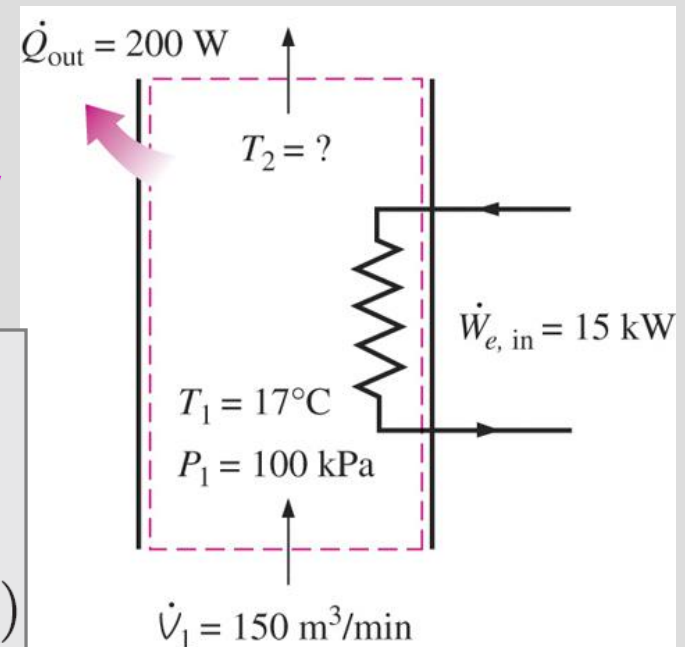
Heat losses from a hot fluid flowing through an uninsulated pipe or duct to the cooler environment may be very significant.

Energy balance for the pipe flow shown in the figure is

$$\begin{aligned}\dot{E}_{in} &= \dot{E}_{out} \\ \dot{W}_{e,in} + \dot{m}h_1 &= \dot{Q}_{out} + \dot{m}h_2 \\ \dot{W}_{e,in} - \dot{Q}_{out} &= \dot{m}c_p(T_2 - T_1)\end{aligned}$$



Pipe or duct flow may involve more than one form of work at the same time.



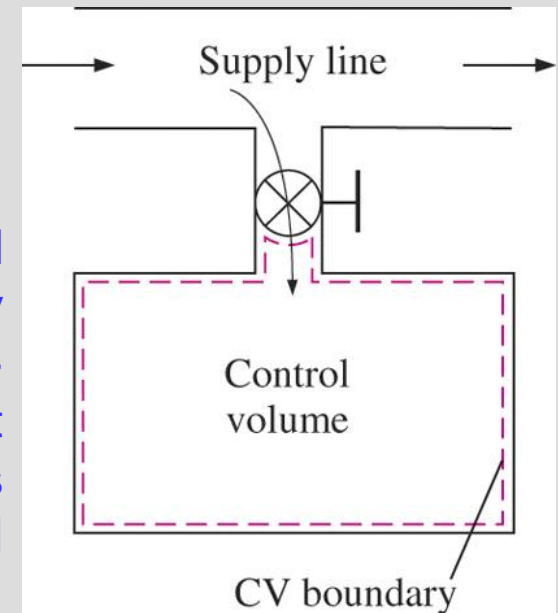
ENERGY ANALYSIS OF UNSTEADY-FLOW PROCESSES

Many processes of interest, however, involve *changes* within the control volume with time. Such processes are called *unsteady-flow*, or *transient-flow*, processes.

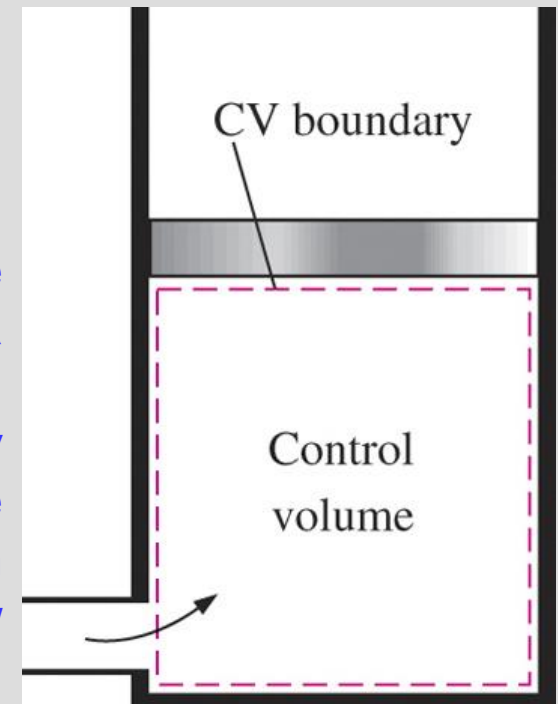
Most unsteady-flow processes can be represented reasonably well by the *uniform-flow process*.

Uniform-flow process: The fluid flow at any inlet or exit is uniform and steady, and thus the fluid properties do not change with time or position over the cross section of an inlet or exit. If they do, they are averaged and treated as constants for the entire process.

Charging of a rigid tank from a supply line is an unsteady-flow process since it involves changes within the control volume.



The shape and size of a control volume may change during an unsteady-flow process.



Mass balance

$$m_{\text{in}} - m_{\text{out}} = \Delta m_{\text{system}} \quad \Delta m_{\text{system}} = m_{\text{final}} - m_{\text{initial}}$$

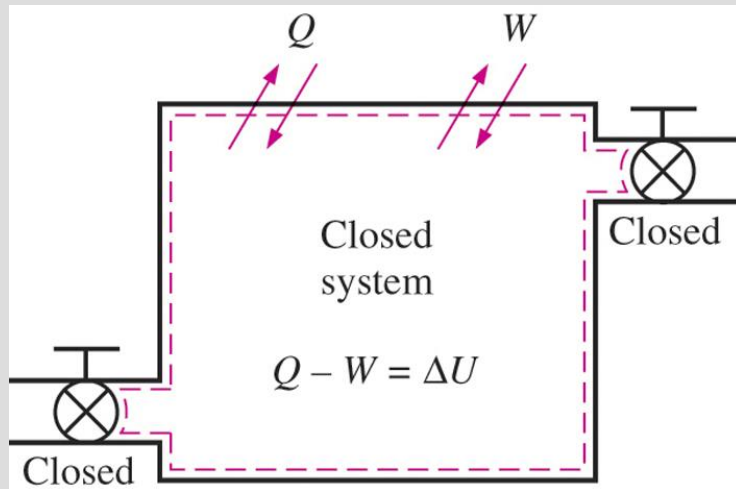
$$m_i - m_e = (m_2 - m_1)_{\text{CV}} \quad i = \text{inlet}, e = \text{exit}, 1 = \text{initial state}, \text{ and } 2 = \text{final state}$$

Energy balance

$$\underbrace{E_{\text{in}} - E_{\text{out}}}_{\text{Net energy transfer by heat, work, and mass}} = \underbrace{\Delta E_{\text{system}}}_{\text{Change in internal, kinetic, potential, etc., energies}}$$

$$\left(Q_{\text{in}} + W_{\text{in}} + \sum_{\text{in}} m\theta \right) - \left(Q_{\text{out}} + W_{\text{out}} + \sum_{\text{out}} m\theta \right) = (m_2 e_2 - m_1 e_1)_{\text{system}}$$

$$\theta = h + \text{ke} + \text{pe} \quad e = u + \text{ke} + \text{pe}$$



The energy equation of a uniform-flow system reduces to that of a closed system when all the inlets and exits are closed.

A uniform-flow system may involve electrical, shaft, and boundary work all at once.

