

King Saud University
Mechanical engineering Department

ME 374 final exam, Thermodynamics tables are allowed, three hour exam, 5-3-1435H, 6-1-2014 G.
Solve questions 1, 2, 3 and 4 then solve only one question, either number 5 or 6.

Question # 1

One kg-mole of n-octane C_8H_{18} (g) at 25 °C is burned with 100 percent excess air at 400 K in a constant pressure steady flow process as seen in Fig. 1. If the products of combustion leave at 700 K,

C_8H_{18} (g) at 25 °C
100% excess air
at 400 K

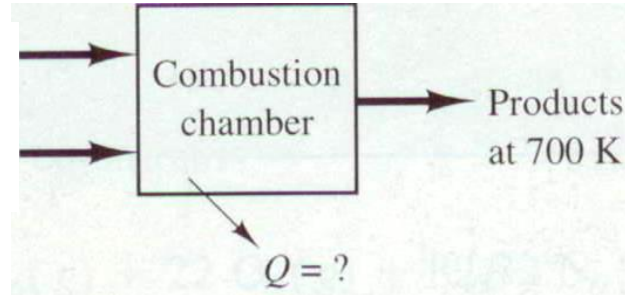


Fig. 1

- (a) Write the balanced stoichiometric combustion equation of the fuel,
- (b) Write the balanced actual combustion equation of the fuel
- (c) Determine the air to fuel ratio of the equation in part (b),
- (d) Determine the amount of heat transferred in part (b)
- (e) If the total pressure of the products is 101 kPa, determine the dew point temperature of the combustion equation in part (b).

Question # 2

- (a) How does useful work differ from actual work? For what kind of systems are these two identical?
- (b) Is the exergy of a system different in different environment?
- (c) A 1.2-m³ insulated rigid tank contains 2.13 kg of carbon dioxide at 100 kPa. Now paddle-wheel work is done on the system until the pressure in the tank rises to 120 kPa. Determine:
 - (1) the actual paddle-wheel work done during this process,
 - (2) the minimum paddle-wheel work with which this process (between the same end states) could be accomplished,
 - (3) the entropy generation, and
 - (4) the surrounding work, and
 - (5) destroyed exergy. Take $T_0 = 298$ K.

Question # 3

- (a) Show that the thermal efficiency of the ideal Brayton cycle under the cold air standard assumptions can be written as:

$$\eta_{th,Brayton} = 1 - \frac{1}{r_p^{(k-1)/k}}$$

Where r_p and k are the pressure ratio and the specific heat ratio respectively.

- (b) An ideal diesel engine has a compression ratio of 20 and uses air as the working fluid. The state of air at the beginning of the **isentropic** compression process is 95 kPa and 20°C. The expansion process is **polytropic** with the polytropic exponent $n = 1.35$. If the maximum temperature in the cycle is not to exceed 2200 K. Assume constant specific heats for air at room temperature, determine.
 - (1) the thermal efficiency,
 - (2) the mean effective pressure, and
 - (3) draw the cycle on a P-V and T-S diagrams.

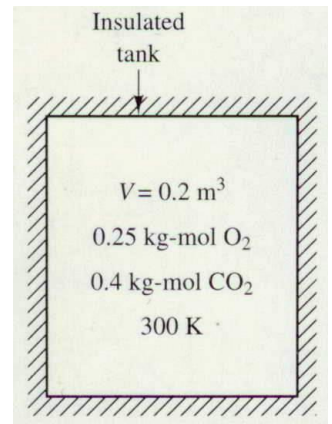
Question # 4

- (a) Prove that for ideal gas mixture; the pressure fraction = the volume fraction = the mole fraction.

$$\frac{P_i}{P_m} = \frac{V_i}{V_m} = \frac{N_i}{N_m} = y_i$$

- (b) An insulated rigid tank of volume 0.2 m³ contains 0.25 kg-mole of O₂ and 0.4 kg-mole of CO₂ at 300 K as shown in the figure. Determine the pressure of the mixture using:

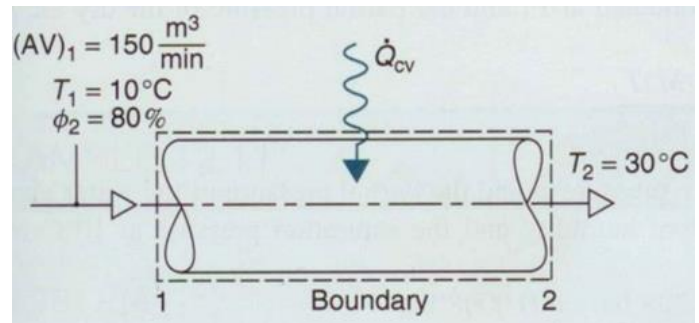
- (1) The ideal gas equation of state
- (2) The compressibility factors based on Amagat's model
- (3) Kay's rule



SOLVE ONLY ONE QUESTION OF THE FOLLOWING

Question # 5

- (a) Show that the relative humidity of the air can be given by $\phi = P_v/P_g$ where P_v and P_g are the vapor pressure of unsaturated and saturated air respectively.
- (b) Moist air enters a duct at 10°C, 80% relative humidity, and a volumetric flow rate of 150 m³/min. The mixture is heated as it flows through the duct and exits at 30°C. No moisture is added or removed, and the mixture pressure remains approximately constant at 100kPa. For steady state operation, determine: (Changes in kinetic and potential energy can be ignored)
- (1) The rate of heat transfer, in kJ/min, and
 - (2) The relative humidity at the exit.
 - (3) Show the process on T-v diagram



Question # 6

Nitrogen gas is compressed from 80 kPa and 27°C to 480 kPa by a 10-kW compressor. Determine the mass flow rate of nitrogen through the compressor, assuming the compression process to be (a) isentropic, (b) polytropic with $n=1.3$, (c) isothermal, and (d) ideal two-stage polytropic with $n=1.3$. Draw a P-V diagram showing all processes from (a) to (d). What is the most desirable process?

Some Relations you may need

$$\underbrace{S_{\text{in}} - S_{\text{out}}}_{\text{Net entropy transfer by heat and mass}} + \underbrace{S_{\text{gen}}}_{\text{Entropy generation}} = \underbrace{\Delta S_{\text{system}}}_{\text{Change in entropy}}$$

$$\underbrace{X_{\text{in}} - X_{\text{out}}}_{\text{Net exergy transfer by heat, work, and mass}} - \underbrace{X_{\text{destroyed}}}_{\text{Exergy destruction}} = \underbrace{\Delta X_{\text{system}}}_{\text{Change in exergy}}$$

$$\begin{aligned}\Delta X &= X_2 - X_1 = m(\phi_2 - \phi_1) = (E_2 - E_1) + P_0(V_2 - V_1) - T_0(S_2 - S_1) \\ &= (U_2 - U_1) + P_0(V_2 - V_1) - T_0(S_2 - S_1) + m \frac{V_2^2 - V_1^2}{2} + mg(z_2 - z_1)\end{aligned}$$

$$\psi_1 - \psi_2 = (h_1 - h_2) - T_0(s_1 - s_2) + \frac{V_1^2 - V_2^2}{2} + g(z_1 - z_2)$$

$$\text{MEP} = \frac{W_{\text{net}}}{V_{\text{max}} - V_{\text{min}}} = \frac{w_{\text{net}}}{V_{\text{max}} - V_{\text{min}}} \quad (\text{kPa})$$

Isentropic compression with $k = 1.4$:

$$w_{\text{comp,in}} = \frac{kRT_1}{k-1} \left[\left(\frac{P_2}{P_1} \right)^{(k-1)/k} - 1 \right]$$

For ideal gases isentropic process between states 1 and 2 we have:

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1} \right)^{(k-1)/k}, \quad \frac{T_1}{T_2} = \left(\frac{V_2}{V_1} \right)^{k-1}$$

$$s_2 - s_1 = \int_1^2 c_v(T) \frac{dT}{T} + R \ln \frac{V_2}{V_1}$$

$$s_2 - s_1 = \int_1^2 c_p(T) \frac{dT}{T} - R \ln \frac{P_2}{P_1}$$

$$\phi = \frac{m_v}{m_g} = \frac{P_v}{P_g}$$

$$\omega = \frac{m_v}{m_a} = \frac{0.622 P_v}{P - P_v} \quad (\text{kg H}_2\text{O/kg dry air})$$

$$h = h_a + \omega h_g \quad (\text{kJ/kg dry air})$$