

- (1) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$, its diffusivity at $P = 1$ atm and $T = 50$ °C will be
- | | |
|--|---|
| (a) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | ✓ (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| (c) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (2) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$, its diffusivity at $P = 0.5$ atm and $T = 25$ °C will be
- | | |
|--|---|
| (a) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| ✓ (c) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (3) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 1$ atm and $T = 25$ °C, molecular diffusivity of 10%-Helium in Nitrogen will be
- | | |
|---|---|
| ✓ (a) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| (c) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (4) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 1$ atm and $T = 25$ °C, molecular diffusivity of 1%-Nitrogen in Helium will be
- | | |
|---|---|
| ✓ (a) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| (c) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (5) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of air in water vapor is $2.6 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of air in liquid water is approximately
- | | |
|---|---|
| (a) $2.2 \times 10^{-2} \text{ m}^2/\text{s}$ | (b) $2.6 \times 10^{-3} \text{ m}^2/\text{s}$ |
| (c) $2.6 \times 10^{-5} \text{ m}^2/\text{s}$ | ✓ (d) $2.2 \times 10^{-9} \text{ m}^2/\text{s}$ |
- (6) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of air in water vapor is $2.6 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 2$ atm and $T = 25$ °C, the molecular diffusivity of air in liquid water is approximately
- | | |
|---|---|
| (a) $2.2 \times 10^{-2} \text{ m}^2/\text{s}$ | (b) $2.6 \times 10^{-3} \text{ m}^2/\text{s}$ |
| (c) $2.6 \times 10^{-5} \text{ m}^2/\text{s}$ | ✓ (d) $2.2 \times 10^{-9} \text{ m}^2/\text{s}$ |
- (7) At a given temperature and pressure, the complete evaporation of a droplet of liquid of 2 mm diameter takes about 300 s approximately. How much time will approximately be required for the complete evaporation of a droplet of water of diameter = 4 mm.
- | | |
|-----------|--------------|
| (a) 150 s | (b) 300 s |
| (c) 600 s | ✓ (d) 1200 s |

Water at 25°C is flowing in a covered irrigation ditch below ground. Every 100 m, there is a vent line 30 mm inside diameter and 1.0 m long to the outside atmosphere at 25°C. There are 10 vents in the 1000-m ditch. The outside air can be assumed to be dry. Calculate the total evaporation loss of water in kg/day. Use the diffusivity data from Table 6.2-1.

$$T = 298 \text{ K}; P = 1.01325 \times 10^5 \text{ Pa}; D_{AB} = 2.6 \times 10^{-5} \text{ m}^2/\text{s};$$

$$\text{Area} = \pi(30/1000)^2 \text{ m}^2 = 7.07 \times 10^{-4} \text{ m}^2$$

$$p_{A1} = 3116 \text{ Pa (Vapor pressure of water vapor at 25°C)}$$

$$p_{A2} = 0 \text{ (Assuming dry air, i.e. no water vapor)}$$

$$p_{B1} = P - p_{A1} = 101.325 \times 10^3 - 3.116 \times 10^3 = 98,159 \text{ Pa}$$

$$p_{B2} = P - p_{A2} = 101.325 \times 10^3 - 0 = 101,325 \text{ Pa}$$

$$p_{BM} = \frac{p_{B2} - p_{B1}}{\ln \frac{p_{B2}}{p_{B1}}} = \frac{p_{A1} - p_{A2}}{\ln \frac{p_{B2}}{p_{B1}}} = 99734 \text{ Pa}$$

$$\text{When, } p_{B1} \approx p_{B2}; p_{BM} \approx \frac{p_{B1} + p_{B2}}{2} = 99742 \text{ Pa}$$

$$N_A = \frac{D_{AB}}{(z_2 - z_1) RT} \frac{P}{p_{BM}} \frac{p_{A1} - p_{A2}}{p_{BM}} = \frac{2.6 \times 10^{-5}}{1.0} \frac{1.01325 \times 10^5 (3116 - 0)}{8314 \times 298 \times 99734} = 3.38 \times 10^{-8} \frac{\text{kg mol}}{\text{m}^2 \cdot \text{s}}$$

$$n_A = N_A \times \text{Area} \times MW \times (s/\text{day}) \times \text{vents}$$

$$= 3.38 \times 10^{-8} \frac{\text{kg mol}}{\text{m}^2 \cdot \text{s}} \times 7.07 \times 10^{-4} \text{ m}^2 \times 18 \frac{\text{kg}}{\text{kg mol}} \times \frac{86400 \text{ s}}{\text{day}} \times 10$$

$$= 3.71 \times 10^{-4} \frac{\text{kg}}{\text{d}}$$

- (1) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$, its diffusivity at $P = 0.5$ atm and $T = 25$ °C will be
- | | |
|--|---|
| (a) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| ✓ (c) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (2) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$, its diffusivity at $P = 1$ atm and $T = 50$ °C will be
- | | |
|--|---|
| (a) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | ✓ (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| (c) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (3) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 1$ atm and $T = 25$ °C, molecular diffusivity of 10%-Helium in Nitrogen will be
- | | |
|---|---|
| (a) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| ✓ (c) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (4) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of 1%-Helium in Nitrogen is given $7 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 1$ atm and $T = 25$ °C, molecular diffusivity of 1%-Nitrogen in Helium will be
- | | |
|---|---|
| (a) $14 \times 10^{-5} \text{ m}^2/\text{s}$ | (b) less than 14×10^{-5} and more than $7 \times 10^{-5} \text{ m}^2/\text{s}$ |
| ✓ (c) $7 \times 10^{-5} \text{ m}^2/\text{s}$ | (d) more than $14 \times 10^{-5} \text{ m}^2/\text{s}$ |
- (5) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of air in water vapor is $2.6 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of air in liquid water is approximately
- | | |
|---|---|
| (a) $2.2 \times 10^{-2} \text{ m}^2/\text{s}$ | (b) $2.6 \times 10^{-3} \text{ m}^2/\text{s}$ |
| (c) $2.6 \times 10^{-5} \text{ m}^2/\text{s}$ | ✓ (d) $2.2 \times 10^{-9} \text{ m}^2/\text{s}$ |
- (6) At a given temperature and pressure, the complete evaporation of a droplet of liquid of 2 mm diameter takes about 300 s approximately. How much time will approximately be required for the complete evaporation of a droplet of water of diameter = 4 mm?
- | | |
|-----------|--------------|
| (a) 150 s | (b) 300 s |
| (c) 600 s | ✓ (d) 1200 s |
- (7) At $P = 1$ atm and $T = 25$ °C, the molecular diffusivity of air in water vapor is $2.6 \times 10^{-5} \text{ m}^2/\text{s}$. At $P = 2$ atm and $T = 25$ °C, the molecular diffusivity of air in liquid water is approximately
- | | |
|---|---|
| (a) $2.2 \times 10^{-2} \text{ m}^2/\text{s}$ | (b) $2.6 \times 10^{-3} \text{ m}^2/\text{s}$ |
| (c) $2.6 \times 10^{-5} \text{ m}^2/\text{s}$ | ✓ (d) $2.2 \times 10^{-9} \text{ m}^2/\text{s}$ |

Water at 25°C is flowing in a covered irrigation ditch below ground. Every 100 m, there is a vent line 20 mm inside diameter and 0.5-m long to the outside atmosphere at 25°C. There are 10 vents in the 1000-m ditch. The outside air can be assumed to be dry. Calculate the total evaporation loss of water in kg/day. Use the diffusivity data from Table 6.2-1.

$$T = 298 \text{ K}; P = 1.01325 \times 10^5 \text{ Pa}; D_{AB} = 2.6 \times 10^{-5} \text{ m}^2/\text{s};$$

$$\text{Area} = \pi(20/1000)^2 \text{ m}^2 = 3.14 \times 10^{-4} \text{ m}^2$$

$$p_{A1} = 3116 \text{ Pa (Vapor pressure of water vapor at 25°C)}$$

$$p_{A2} = 0 \text{ (Assuming dry air, i.e. no water vapor)}$$

$$p_{B1} = P - p_{A1} = 101.325 \times 10^3 - 3.116 \times 10^3 = 98,159 \text{ Pa}$$

$$p_{B2} = P - p_{A2} = 101.325 \times 10^3 - 0 = 101,325 \text{ Pa}$$

$$p_{BM} = \frac{p_{B2} - p_{B1}}{\ln \frac{p_{B2}}{p_{B1}}} = \frac{p_{A1} - p_{A2}}{\ln \frac{p_{B2}}{p_{B1}}} = 99734 \text{ Pa}$$

$$\text{When, } p_{B1} \approx p_{B2}; p_{BM} \cong \frac{p_{B1} + p_{B2}}{2} = 99742 \text{ Pa}$$

$$N_A = \frac{D_{AB}}{(z_2 - z_1) RT} \frac{P}{p_{BM}} \frac{p_{A1} - p_{A2}}{p_{BM}} = \frac{2.6 \times 10^{-5}}{0.5} \frac{1.01325 \times 10^5 (3116 - 0)}{8314 \times 298} \frac{1}{99734} = 6.75 \times 10^{-8} \frac{\text{kg mol}}{\text{m}^2 \cdot \text{s}}$$

$$n_A = N_A \times \text{Area} \times MW \times (\text{s/day}) \times \text{vents}$$

$$= 6.75 \times 10^{-8} \frac{\text{kg mol}}{\text{m}^2 \cdot \text{s}} \times 3.14 \times 10^{-4} \text{ m}^2 \times 18 \frac{\text{kg}}{\text{kg mol}} \times \frac{86400 \text{ s}}{\text{day}} \times 10$$

$$= 3.30 \times 10^{-4} \frac{\text{kg}}{\text{d}}$$